

# Anode Catalyst Development for Direct Formic Acid Fuel Cell

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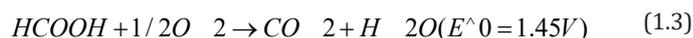
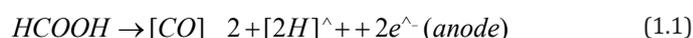
## Abstract

Extensive studies have been reported on improving the performance of direct formic acid fuel cell (DFAFC) including the catalyst layer in which the electrochemical reaction takes place. This review is focusing on the anode catalysts development to improve the electrocatalytic performance for formic acid oxidation reaction (FAOR) including the modification on the metal and support of the catalyst. These efforts are contributing in the enhancing the catalyst electrocatalytic performance and reducing the usage of high cost catalyst material which is beneficial for commercialization purpose.

**Keywords:** Formic acid oxidation reaction; Anode catalyst; Catalyst support

## Introduction

Direct formic acid fuel cell (DFAFC) is one of the promising direct liquid fuel cell (DLFC) due to its capabilities of favorable oxidation kinetics enabling low operating temperatures (50-80 °C), high theoretical open circuit voltage (1.45V) and relatively low fuel crossover through Nafion membrane due to repulsion between HCOO<sup>-</sup> ions in formic acid and sulfuric group in Nafion membrane [1-3]. Basically, DFAFC uses formic acid to generate electricity without intermediate step such as reforming the alcohol into hydrogen. Liquid formic acid is easily found and approved by the US Food and Drug Administration (FDA) as a food additive. Formic acid electro-oxidation occurs via a dual reaction pathway that reduce the percentage of poisoning toward the surface as intermediate reaction [4]. Redox reaction of formic acid as shown in the Equation 1.1 for the anode and cathode reaction.



Principally, DFAFCs are subcategory of polymer electrolyte membrane fuel cells (PEMFCs) in which formic acid as aqueous solution instead of hydrogen. At the anode, formic acid solution diffuses through the diffusion layer and the catalyst layer where solution is electrochemically oxidized into carbon dioxide (CO<sub>2</sub>) and two electrons compared to direct methanol fuel cell (DMFC) which generates six electrons. This means that at a same current density, DFAFC requires two times amount of fuel [5]. Like most of other DLFCs, chemical used in DFAFCs also release CO<sub>2</sub> in the reaction which is not completely safe and not emission-free. However, CO<sub>2</sub> can be converted into various valuable chemicals such as formic acid through electrochemical reduction and can be reused in DFAFC [6]. The CO<sub>2</sub> generated from the oxidation reactions emerges from the anode backing layer as bubbles and is removed via the flowing aqueous formic acid solution. Protons formed during this reaction diffuse through the electrolyte membrane to the cathode layer. Likewise, in the DMFC, electrons and protons combine with oxygen to form water at cathode. As the components of DFAFC are similar to the DMFC, except for the anode catalyst, development of anode catalyst for DFAFCs have drawn considerably attention by many researchers. Hence, the objective of this paper is to review the anode catalysts development to improve the electrocatalytic performance for formic acid oxidation reaction (FAOR) including the modification on the metal and support of the catalyst.

## Anode catalyst development

In DFAFC operation, palladium- (Pd) or platinum- (Pt) based catalysts are the most utilized as the anode catalyst for formic acid oxidation reaction (FAOR) but, Pd-based is

regarded as more active than Pt-based. This is due to the less carbon monoxide (CO) poisoning on the Pd than Pt. Formic acid electrooxidation on Pd-based catalyst usually proceeds on a direct pathway (dehydrogenation) in which formic acid is oxidized to CO<sub>2</sub> without forming CO [7]. FAOR on a Pt-based catalyst follows the so-called dual pathways of dehydrogenation and the indirect reaction pathway that forms adsorbed CO as an intermediate reaction. This intermediate reaction will lead to Pt poisoning by CO and reduce its electrocatalytic performance [8]. Pt-based catalysts have been widely developed to improve the electrocatalytic performance [9]. The application of bimetallic alloys such as Pt-Ru, Pt-Pd, Pt-Au, Pt-Bi [10-12] was found to exhibit better electrocatalytic activity than the pure noble metals for FAOR. In a study done by C. Rice et al., the behavior of Pt black, Pt-Ru and Pt-Pd catalyst under a real fuel cell operation was reported. It was concluded that the addition of Pd to the Pt catalyst improves the formic acid electrooxidation rate via direct reaction pathway whereas addition of Ru to the Pt enhances the electrooxidation via indirect reaction pathway that forming CO intermediates [10].

A recent study done by Choi et al. [13] to improve the FAOR of the Pt-based catalyst is by using a simple and easy method to prepare Bi-modified Pt/C catalyst in which the Bi was reversibly adsorbed on a commercial Pt/C catalyst. The Bi-modified Pt/C catalyst demonstrates an excellent FAOR activity as compared with the non-modified Pt/C catalyst. Further, single-cell performance was improved using the Bi-modified Pt/C as the anode catalyst with a power density of over 2.5 times that of the commercial Pt/C and Pt black anode catalyst. In addition, they also successfully manufactured a DFAFC stack that delivered 300 W power by employing the Bi-modified Pt/C at the cathode which is expected to contribute to the commercialization of DFAFC [13]. To date, extensive studies are also reported on Pd-based catalyst for formic acid electro-oxidation due to its high anti-poisoning ability than Pt-based catalyst. However, a major problem of Pd-based catalysts is their poor electrocatalytic stability. Alloying the Pd with other metal (Ni, Zn, V, Au, Co) or element is one of the efforts to improve the electrocatalytic activity and stability. Carbon supported Pd-Ni (Pd-Ni/C) catalyst was found to be better in the electrocatalytic activity and stability than the Pd/C catalyst due to the decrease in the decomposition of formic acid as shown in the study done by Shen et al. [14].

From the recorded volume of gas produced from the formic acid decomposition over the catalyst, it was found that gas volume produced for the Pd-Ni/C catalyst are much less than that of Pd/C catalyst. This finding indicates that Pd-Ni/C catalyst can fully prevent the formic acid decomposition and reduce the CO production which contribute in the improved electrocatalytic activity and stability of the Pd-Ni/C catalyst for FAOR [14]. Similar trend obtained by Fathirad [15] in which the electrocatalytic activity and stability of carbon supported Pd-Zn (Pd-Zn/C) catalyst is better than Pd/C catalyst. They also proved that the different atomic ratio affects the formic acid electrooxidation and stability of a Pd-Zn/C catalyst. The electroactivity increases as the Pd/Zn atomic ratio increases up to 65.2:34.8 (Pd<sub>2</sub>Zn/C). Further increase in the metal atomic ratio

results in decrease of the electroactivity of the Pd-Zn/C catalyst. It was reported that the Pd<sub>2</sub>Zn/C catalyst has the smallest average crystallite size (8.2nm) and largest electrochemical surface area. [15]. Another factor that was proved to affect the electrocatalytic activity and stability of Pd-based alloy catalyst is the alloying degree. Carbon supported Pd-Au (Pd-Au/C) catalyst with high and low alloying degree prepared by the co-reduction of Pd and Au salt precursor in aqueous solution with or without tetrahydrofuran (THF) in the study reported by Zhang et al. [16] High alloy degree Pd-Au/C catalyst shows a higher activity and stability for FAOR than that low alloying degree catalyst. This is because the high alloying degree catalyst has better CO tolerance and possible suppression of dehydration pathway for formic acid electrooxidation [16].

Different second metal added to the Pd-based catalyst also affects the FAOR activity and stability and the single DFAFC performance. Caglar et al. [17] synthesized and characterized carbon nanotube (CNT) supported Pd-Co, Pd-V, Pd-Mn and Pd-Zn catalysts for formic acid electrooxidation activity and stability. Pd-Co/CNT catalyst exhibited the best activity and stability than the other catalysts including the Pd/CNT catalyst [17]. Instead of alloying Pd with other metals, Zhang et al. [18] prepared a highly active and stable Pd hydride (PdH<sub>x</sub>) catalyst by simply treating a commercial Pd black with n-butylamine in solvothermal condition. As compared with the untreated commercial Pd black catalyst, the PdH catalyst exhibited a very low peak potential, a high mass activity and greater catalytic stability towards the formic acid electrooxidation. In addition, the preparation method used can be regarded as facile and cost-effective which is suitable for practical application [18]. Table 1 shows the summary of electrocatalytic performance of current studies on the Pd-based catalyst for FAOR. From the literatures discussed here, it can be concluded that addition of second metal or element to the Pd/C catalyst can successfully improve the electrocatalytic activity and stability for FAOR.

**Table 1:** Electrocatalytic activity result of Pd-based catalyst for FAOR.

Reference	Catalyst	Anodic Peak Potential (mV)	Peak Current Density (mA cm <sup>-2</sup> )
Zhang et al. [16]	Pd-Au/C Pd/C	15	19
		24	12.4
Shen et al. [14]	Pd-Ni/C Pd/C	22	19.3
		12	0.95
Fathirad [15]	Pd-Zn/C Pd/C	~30	~20
		~35	~9
Zhang et al. [18]	PdH Pd black	4	5.12
		22	1.02
Caglar et al. [7]	Pd-Co/ CNT Pd/CNT	200 -400	6.89
		-	0.68

Besides alloying the Pd-based catalyst with the other non-noble metal or other element, the electrocatalytic performance toward the FAOR can be improved by development of catalyst support structure. Supported catalyst can reduce the usage of expensive metal catalyst simultaneously improving the catalyst electroactivity [19,20]. Desired supported catalysts are expected to have high surface area, good electrical conductivity, electrochemical stability and suitable porosity shows good stability, good interaction as a catalyst support, the ability to repel water and prevent flooding, corrosion resistance, easily restore catalyst function and higher activity than unsupported catalyst [20-25]. Unsupported catalysts suffer aggregation and surface area degradation during catalytic reaction took place [26], however the investigation of unsupported catalyst could provide the understanding on the catalytic activity on specific catalyst [27].

Support material have been roughly classified as carbon-based support and non-carbon-based support [20]. Among non-carbon-based material that attract researchers attention were titania [28-31], alumina, silica [28], ceria [30], zirconia, tungsten oxide and conducting polymers [20]. Non-carbon support improved the reaction kinetics due to the metal-support interaction, however, their electrical conductivity was lower than that of the carbon support. The lower electrical conductivity should be improved when non-carbon support is used as catalyst support, and this was pointed out by Ito et al. [29] & Kunitomo et al. [30]. In their studies, the non-carbon supported PtRu catalyst, such as ceria particles [30] and titania particles [29], gave lower performance for methanol oxidation comparing to the carbon support.

Carbon based support such as carbon blacks (CBs) such as Vulcan XC-72, Ketjen black, etc., [22] and novel nanostructured carbon such as carbon nanotube (CNT) [7,32-34], carbon nanofiber (CNF), carbon microbeads and carbon nanocoils [35] graphene [26] and mesoporous carbon [20,36] are widely used in low temperature fuel cells. Nanostructured carbon support seems to enhance catalyst activity due to its high surface areas which increases reaction surface areas of catalyst [37]. Carbon based material is favored as catalyst support due to its properties of high electrical conductivity, corrosion resistance, porous structure and specific surface area. These properties are differ based on the carbon materials. Usually high specific surface area is needed to serve high dispersion of catalyst particles; however, high specific surface area only is inadequate as efficient catalyst support. Pore properties such as pore size and distribution and surface chemistry are also important to take into account [38]. Carbon nanostructure not only reduce the cost of fuel cell operation by reducing the catalyst loading but also contributed to high performance due to catalytic reaction occurred at the active sites [39].

## Conclusion

In summary, the electrocatalytic performance improvement of anode catalyst for formic acid oxidation reaction (FAOR) can be realized either on the metal (Pt or Pd) or the support material. Addition of second metal or element to the Pt- or Pd-based catalysts was found to enhance the electro-oxidation of formic acid and

stability of the catalysts. This is due to the increase the ability of the catalyst to proceed in the direct reaction pathway and CO tolerance. Further, the modification on the catalyst support material also leads in the change of physical properties and the metal support interaction which contribute in improving the electrocatalytic performance.

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