

# Isotherm Modeling and Thermodynamic Study of the Adsorption of Toxic Metal by the Apricot Stone

Moussa Abbas<sup>1\*</sup>, Tounsia Aksil<sup>1</sup> and Mohamed Trari<sup>2</sup>

<sup>1</sup>Laboratory of Soft Technologies and Biodiversity, M'Hamed Bouguerra University of Boumerdés, Algeria

<sup>2</sup>Laboratory of Storage and Valorization of Renewable Energies, University of Science and Technology Houari Boumediene, Algeria

\*Corresponding author: Moussa Abbas, Laboratory of Soft Technologies and Biodiversity, Faculty of Science, M'Hamed Bouguerra University of Boumerdés, Algeria

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## Abstract

The adsorption of Lead onto apricot stone activated carbon (ASAC) in a batch adsorber has been studied. The adsorbent was characterized by FTIR, BET, X-fluorescence, X-ray diffraction and SEM. The effects of contact time, initial pH, agitation speed, adsorbent dosage and initial dye concentration on the Lead adsorption by the ASAC have been studied. Lead removal was seen to increase with increasing contact time until equilibrium and initial dye concentration, and the adsorption capacity of ASAC selected to follow the adsorption process. Batch adsorption experiments were first undertaken to assess the effect of various parameters on the removal efficiency of Lead. It was observed that under optimized conditions up to 166.813mg/g at 25 oC at pH 8 could be removed from solution. Kinetic parameters; rate constants, equilibrium adsorption capacities and correlation coefficients, for each kinetic equation were calculated and discussed. It was shown that the adsorption of Lead onto ASAC could be described by the pseudo second-order equation. The experimental isotherm data were analyzed using the Langmuir, Freundlich and Temkin equations. Adsorption of Lead onto ASAC followed the Freundlich isotherm. The evaluation of thermodynamics parameters indicated respectively the spontaneous and endothermic nature of the reaction and the chemisorption of the sorption process.

**Keywords:** Apricot stone; Heavy metal; Isotherm; Removal; Thermodynamic

## Introduction

The effects of heavy metals like lead, mercury, copper, zinc and cadmium on the human health have been extensively studied and well documented. Excessive ingestion of such metals can cause accumulative poisoning, cancer, nervous system damage. We are interesting by lead which is ubiquitous in the environment and hazardous at high level and its location in the world is reported in. It is a general metabolic poison and enzyme inhibitor and can accumulate in bones, brain, kidney and muscles. Long-term drinking water containing lead causes serious disorders, like anemia, kidney disease and mental retardation. Effluents contaminated by heavy metals are commonly produced from many industrial processes and the residues in contaminated habitats may accumulate in microorganisms, aquatic flora and fauna, which in turn, enter into the human body through the food chain, thus resulting in health problems. So its removal from aqueous medium is necessary because of frequent appearance of this metal in wastewaters from industrial activities. Lead is a common industrial metal that has become widespread in air, water and soil Table 1.

**Table 1:** Location of lead in the world in 2004.

Continent	Production (Tonnes)	Consumption (Tonnes)
Asia	2880000	2870000
Americas	2009000	2030000
Europe	1551000	2011000
Africa	101000	131000
Oceania	281000	40000

Lead is widely used in the storage batteries, gasoline additives and other chemicals, ammunition (shot and bullets), solder, and other uses and the world production exceeds 3 million tons per year. The presence of heavy metals in the aquatic environment has been of great concern for the scientists and engineers because of their increased discharge, toxic nature, and other adverse effects on receiving waters. In this respect, the excessive utilization of lead has dramatically raised its concentration in blood. In order

to insure a better quality of life and protect the environment, removing lead from industrial wastes is of vital importance. Unlike organic compounds, lead is non-biodegradable and, therefore, must be removed from water. Agricultural by-products exist in large amounts and about 20,000 tonnes of apricot stones per year are produced in Algeria [1], which represents consequently a solid pollutant to the environment.

Over the past, these by-products were used as fuel in rural areas but now the preparation of activated carbon is considerably encouraged. Apricot stone is a cheap precursor for activated carbon source. Therefore, it is important to evaluate its performance as adsorbent. The advantages of the adsorption reside in the simplicity of the operation, low cost compared to other separation methods and no sludge, the adsorption on activated carbon is an efficient and economic processes. Therefore, this study deals with the adsorption ability of ASAC [2-5] for the removal of lead from synthetic aqueous solutions. The influence of the operating parameters such as initial  $Pb^{2+}$  concentration, pH, temperature, adsorbent dosage, particle size and contact time on ASAC is explored [6].

## Experimental

### Batch mode adsorption studies

The effects of the experimental parameters such as, the initial  $Pb^{2+}$  concentration (20-100mg/L), pH (2-14), adsorbent dosage (5-45g/L) and temperature (298-323K) on the adsorptive removal of  $Pb^{2+}$  is studied in batch mode for a specific period of contact time (0-90min). The stock solution is prepared by dissolving the accurate amount of  $PbSO_4 \cdot 7H_2O$  (99%, Merck) in distilled water and other solutions are prepared by dilution. pH is adjusted with HCl (0.1) or NaOH (0.1M). For the kinetic studies, desired quantity of ASAC is contacted with 20mL of  $Pb^{2+}$  solutions in Erlenmeyer flasks. The flasks are then placed on a rotary shaker at 250rpm and the samples are taken at regular time

intervals and centrifuged (3000rpm, 10min). The  $Pb^{2+}$  content in the supernatant is determined using Flame Atomic Absorption Spectrometry (FAAS, model Perkin Elmer 2380). The amount of  $Pb^{2+}$  adsorbed on activated carbon  $q_t$  (mg/g) is calculated by using the following equation (A1):

$$q_t = \frac{(C_0 - C_t) \cdot V}{m} \quad A(1)$$

Where  $C_0$  is the initial  $Pb^{2+}$  concentration and  $C_t$  the  $Pb^{2+}$  concentrations (mg/L) at any time,  $V$  the volume of solution (L) and  $m$  the mass of the activated carbon (g). The  $Pb^{2+}$  removal percentage is calculated from the following equation (A2):

$$R(\%) = \frac{(C_0 - C_t)}{C_0} \cdot 100 \quad A(2)$$

### Adsorption kinetics

The kinetic study is important for the adsorption process because it describes the uptake rate of adsorbate, and controls the residual time of the whole process. Two kinetic models namely the pseudo first order and pseudo second-order are selected in this study for describe the adsorption process. The pseudo first order equation is given by:

$$\log(q_e - q_t) = \log q_e - \frac{K_1}{2.303} \cdot t \quad A(3)$$

While the pseudo second order model is given by:

$$\frac{t}{q_t} = \frac{1}{K_2 \cdot q_e^2} + \frac{1}{q_e} \cdot t \quad A(4)$$

Where  $q_t$  ( $mg \cdot g^{-1}$ ) is the amount of ions adsorbed on ASAC at the time  $t$  (min).  $K_1$  ( $min^{-1}$ ) and  $K_2$  ( $g \cdot mg^{-1} \cdot min^{-1}$ ) are the pseudo-first order and pseudo-second order kinetics constants respectively. For the pseudo-first-order kinetic, the experimental data deviate from linearity, as evidenced from the low values of  $q_e$  and  $C_0$ . Therefore, the pseudo-first order model is inapplicable for this system. By contrast, the correlation coefficient and  $q_{e,cal}$  determined from the pseudo-second order kinetic model are in good agreement with the experimental results Table 2.

**Table 2:** Pseudo-first order and pseudo-second order kinetic model constants.

Pseudo-Second Order Kinetic				Pseudo-First Order Kinetic			
Co (mg/L)	qe, exp (mg/g)	qe, cal (mg/g)	K <sub>2</sub> (g/mgmin)	R <sup>2</sup>	qe cal (mg/g)	K <sub>1</sub> (mn <sup>-1</sup> )	R <sup>2</sup>
30	6.250	6.27	1.499	0.999	0.583	0.139	0.950
40	8.300	8.33	2.996	0.999	0.731	0.312	0.884
80	16.39	16.72	0.299	0.999	1.184	0.117	0.829
100	20.01	20.92	0.524	0.999	1.045	0.096	0.897

### Adsorption isotherms

The shape of the isotherms is the first experimental tool to diagnose the nature of a specific adsorption. The isotherms are generally classified in four main groups: L, S, H, and C shapes

according to of Giles et al [7]. In our case the isotherm of  $Pb^{2+}$  on ASAC displays an L shape [8]. The initial part of the L curve indicates small interaction between  $Pb^{2+}$  and the adsorption sites at low concentrations but when the concentration  $C_0$  in the liquid phase increases, the adsorption occurs more readily. Such behaviour is



due to a synergistic effect with the adsorbed  $Pb^{2+}$ , facilitating the adsorption of additional ions as a result of attractive interactions

adsorbate-adsorbate. The constants parameters are represented in Table 3.

**Table 3:** Sorption isotherm coefficients for different models.

Model	Langmuir	Freundlich	Temkin
	$1/C_e = f(1/q_e)$	$\ln q_e = f(\ln C_e)$	$q_e = f(\ln C_e)$
	$q_{max} = 166.813 \text{ mg/g}$ $K_L = 0.01612 \text{ L/mg}$	$1/n = 0.91345$ $K_F = 2.7456 \text{ mg/g}$	$B = RT/b = 9.17196$ $B = 267.59 \text{ J/mol}$ $B \ln A = 2.7456$ $A = 1.033$
$R^2$	0.9973	0.99078	0.90787
RMSE	3.0032	2.81354	3.4907
SSE	9.0191	7.91601	18.1849
$\chi^2$	0.1011	0.1026	0.2072

## Conclusion

The present study has shown that the activated carbon prepared from apricot stone can be employed as effective and low cost adsorbent for the removal of  $Pb^{2+}$  in aqueous solution. Increasing the initial concentration and pH led to an improved adsorption capacity of ASAC. The Freundlich model provides the best fit of the equilibrium adsorption data with a maximum adsorption capacity of 166.813 mg/g at pH ~8. The positive thermodynamic parameters indicate that the  $Pb^{2+}$  adsorption onto ASAC is endothermic and not spontaneous. The  $Pb^{2+}$  uptake follows the pseudo-second-order kinetic model, which relies on the assumption that the chemisorption is the rate-limiting step. The enthalpy ( $H_o$ , 40 kJ/mol) clearly indicates that  $Pb^{2+}$  is strongly attached to the adsorbent surface by forming chemical bond and tends to find sites that maximize their coordination number with the surface.

The results of the present investigation showed that ASAC is a potentially useful adsorbent for the adsorption of metals, an issue of environmental concern and the natural abundance of this food waste can provide an adsorption medium which contributes to the treatment of wastewater. The comparison of the adsorption capacity of the prepared adsorbent with other adsorbents shows its attractive properties from industrial and economic interests. The study in tiny batch gave rise to encouraging results, and we wish to achieve the adsorption tests in column mode under the

conditions applicable for the treatment of industrial effluents. This work has been undertaken in the field of the environment to evaluate the application potential of activated carbon prepared from apricot stone as a low-cost adsorbent for the removal of toxic pollutants. Pollutant wastewater has long been a major environmental problem all over the world. The problem is further aggravated by rapid industrialization, population growth and unskilled use of natural water resources.

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